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**Analysis of the most important
processes impact on the concentration
reduction values for the chosen
contaminants moving in groundwater
(based on computational solutions)**

The basic simplified assumptions

- Leaving out of advection terms ($u_y \partial C / \partial y = u_z \partial C / \partial z = 0$) for one – dimensional flow of groundwater in x direction ($u_y = u_z = 0$)
- Leaving out of transverse dispersion term ($D_z \partial^2 C / \partial z^2 = 0$) in z direction for slotted contaminant outflow and initial concentration equalization in this direction
- Leaving out of molecular diffusion process due to low values of molecular diffusion coefficients (D_M) in relation to values of dispersion rates (D_x and D_y)
- Leaving out of turbulent diffusion process (D_B) for laminar groundwater flow in sandy ground medium (low graining)

The most simplified well-known 2D advection-dispersion equation without adsorption process:

$$\frac{\partial C}{\partial t} + u_x \frac{\partial C}{\partial x} = D_x \frac{\partial^2 C}{\partial x^2} + D_y \frac{\partial^2 C}{\partial y^2} \quad (1)$$

C – the solute concentration in flowing groundwater in aqueous phase (in the local equilibrium conditions),

u_x – the component of the average (real) seepage velocity in pore space along the x axis (as pore velocity),

D_x – the component of the longitudinal dispersion coefficient along the x axis,

D_y – the component of the transverse dispersion coefficient along the y axis,

t – the co-ordinate of time,

x, y – the co-ordinates of the assumed reference system.

The well-known 2D advection-dispersion equation with adsorption process:

$$\frac{\partial C}{\partial t} \left(1 + \frac{\rho}{m} \frac{\partial S}{\partial C} \right) + u_x \frac{\partial C}{\partial x} = D_x \frac{\partial^2 C}{\partial x^2} + D_y \frac{\partial^2 C}{\partial y^2} \quad (2)$$

S – the mass of the solute species adsorbed on the grounds per unit bulk dry mass of the porous medium (in the local equilibrium conditions),

ρ – the bulk density of the porous medium ,

m – the effective porosity of the porous medium,

$[1+(\rho/m) (\partial S/\partial C)]$ – the constant in time retardation factor (R) resulting from sorption process.

The general equation describing retardation factor for adsorption process (as the Freundlich non-linear isotherm) takes the form:

$$R = 1 + \frac{\rho}{m} \cdot \frac{\partial S}{\partial C} = 1 + \frac{\rho}{m} \cdot N \cdot K \cdot C^{(N-1)} \quad (3)$$

K, N – the parameters of the Freundlich non-linear isotherm accepted for mathematical description of adsorption process for all the chosen in this paper indicators.

The well-known 2D advection-dispersion equation with biodegradation – biological denitrification and adsorption processes:

$$\frac{\partial C}{\partial t} \left(1 + \frac{\rho}{m} \frac{\partial S}{\partial C} \right) + u_x \frac{\partial C}{\partial x} = D_x \frac{\partial^2 C}{\partial x^2} + D_y \frac{\partial^2 C}{\partial y^2} - k_1 \left(C - \frac{\rho S}{m} \right) \quad (4)$$

k_1 – the first-order reaction rate for the kinetically-controlled biodegradation – biological denitrification process (in this analysis the same k_1 parameter was assumed for both the dissolved-aqueous and the sorbed-solid phase.

The well-known 2D advection-dispersion equation with radioactive decay and adsorption processes:

$$\frac{\partial C}{\partial t} + u_x \frac{\partial C}{\partial x} = D_x \frac{\partial^2 C}{\partial x^2} + D_y \frac{\partial^2 C}{\partial y^2} - \frac{\rho}{m} \frac{\partial S}{\partial t} - \lambda \left(C - \frac{\rho S}{m} \right) \quad (5)$$

λ – the first-order decay rate usually expressed as a half-life ($t_{1/2}$) (for radioactive decay we can assume that the reaction generally occur at the same rate for both the dissolved-aqueous and the sorbed-solid phase.

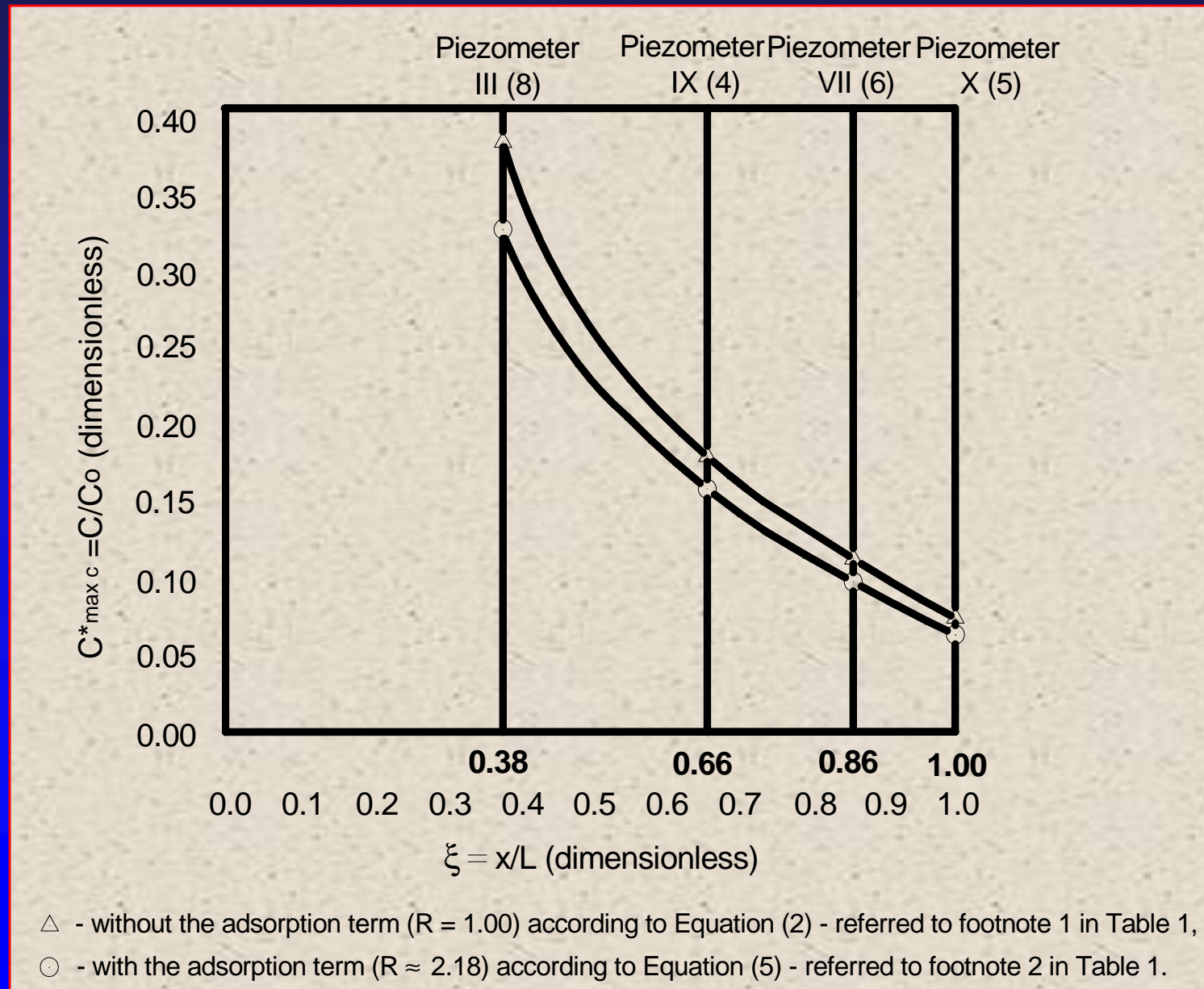
Maximal dimensionless values of the chosen contaminant concentrations (C^*_{maxc}) calculated in relation to appropriate equations:

Chosen contamination in relation to considered processes	Numbers of chosen piezometers with dimensionless and dimensional distances the leakage source in lagoon 4 [total distance L to piezometer X (5)]			
	III (8) 0.38 x \approx 40.0 m	IX (4) 0.66 x \approx 70.0 m	VII (6) 0.86 x \approx 90.0 m	X (5) 1.00 x (L) \approx 105.0 m
Chlorides (NaCl) [adsorption process]	0.4394 ¹⁾ 0.4035 ²⁾ 1.00 ^{a)}	0.2536 ¹⁾ 0.2383 ²⁾ 1.00 ^{a)}	0.1837 ¹⁾ 0.1758 ²⁾ 1.00 ^{a)}	0.0939 ¹⁾ 0.0910 ²⁾ 1.00 ^{a)}
Sulfates (Na₂SO₄) [adsorption process]	0.3846 ¹⁾ 0.3276 ²⁾ 1.00 ^{a)}	0.1795 ¹⁾ 0.1584 ²⁾ 1.00 ^{a)}	0.1129 ¹⁾ 0.0978 ²⁾ 1.00 ^{a)}	0.0743 ¹⁾ 0.0634 ²⁾ 1.00 ^{a)}
Nitrates (NO₃⁻) [biodegradation process]	0.4983 ²⁾ 0.4979 ³⁾ 1.00 ^{a)}	0.2171 ²⁾ 0.2145 ³⁾ 1.00 ^{a)}	0.1040 ²⁾ 0.1031 ³⁾ 1.00 ^{a)}	0.0335 ²⁾ 0.0333 ³⁾ 1.00 ^{a)}
BOD indicator [biodegradation process]	0.6524 ²⁾ 0.6504 ³⁾ 1.00 ^{a)}	0.5252 ²⁾ 0.5242 ³⁾ 1.00 ^{a)}	0.3534 ²⁾ 0.3524 ³⁾ 1.00 ^{a)}	0.2126 ²⁾ 0.2116 ³⁾ 1.00 ^{a)}
Chosen radionuclide [radioactive decay]	0.4035 ²⁾ 0.3879 ⁴⁾ 1.00 ^{a)}	0.2383 ²⁾ 0.2308 ⁴⁾ 1.00 ^{a)}	0.1758 ²⁾ 0.1708 ⁴⁾ 1.00 ^{a)}	0.0910 ²⁾ 0.0895 ⁴⁾ 1.00 ^{a)}

Dimensionless standard error values (Δ/C^*_{maxc}) in relation both to chosen contaminant and to appropriate equations:

Chosen contamination in relation to considered processes	Numbers of chosen piezometers with dimensionless and dimensional distances the leakage source in lagoon 4 [total distance L to piezometer X (5)]			
	III (8) 0.38 x \approx 40.0 m	IX (4) 0.66 x \approx 70.0 m	VII (6) 0.86 x \approx 90.0 m	X (5) 1.00 x (L) \approx 105.0m
Chlorides (NaCl) [adsorption process]: Δ / C^*_{maxc} eq. (2) \times 100% $\Delta = C^*_{maxc} [\text{eqs. (1) - (2)}] $	6.5 ¹⁾	5.3 ¹⁾	3.9 ¹⁾	2.7 ¹⁾
Sulfates (Na₂SO₄) [adsorption process]: Δ / C^*_{maxc} eq. (2) \times 100% $\Delta = C^*_{maxc} [\text{eqs. (1) - (2)}] $	14.4 ¹⁾	10.7 ¹⁾	7.8 ¹⁾	6.0 ¹⁾
Nitrates (NO₃⁻) [biodegradation process]: Δ / C^*_{maxc} eq. (4) \times 1000 ‰ $\Delta = C^*_{maxc} [\text{eqs. (2) - (4)}] $	9.8 ²⁾	8.7 ²⁾	6.2 ²⁾	0.8 ²⁾
BOD indicator [biodegradation process]: Δ / C^*_{maxc} eq. (4) \times 1000 ‰ $\Delta = C^*_{maxc} [\text{eqs. (2) - (4)}] $	4.7 ²⁾	3.3 ²⁾	2.5 ²⁾	2.0 ²⁾
Chosen radionuclide [radioactive decay]: Δ / C^*_{maxc} eq. (5) \times 100% $\Delta = C^*_{maxc} [\text{eqs. (2) - (5)}] $	4.0 ³⁾	3.2 ³⁾	2.9 ³⁾	1.8 ³⁾

Maximal values of dimensionless calculated sulfate concentrations (Na_2SO_4) in the chosen piezometers



Final results of numerical calculations:

- the standard errors between the maximum dimensionless concentrations based on eqs. (2) and (1) (with and without adsorption process) are: from 2.7 to 6.5 for chlorides and from 6.0 to 14.4 for sulfates (as the maximal errors) (values referred to footnote 1 in Table 2, in %),
- the standard errors between the maximum dimensionless concentrations based on eqs. (4) and (2) (with and without biodegradation process and with adsorption in both cases) are: from 0.8 to 9.8 for nitrates and from 2.0 to 4.7 for the BOD indicator (as the minimal errors) (values referred to footnote 2 in Table 2, in ‰),
- the standard errors between the maximum dimensionless concentrations based on eqs. (5) and (2) (with and without radioactive decay and with adsorption in both cases) are: from 1.8 to 4.0 for the chosen radionuclide (values referred to footnote 3 in Table 2, in %).

General conclusions

- 1) **Basing on the numerical calculations, one can say that the non-linear adsorption process is of a very great importance in terms of the concentration reduction, especially for the sulfates and in less range for the chlorides moving in a natural aquifer,**
- 2) **Basing on the numerical calculations, one can say that the biodegradation of the chosen compounds (as nitrates and the BOD indicator) moving in a natural groundwater is of a very small importance in terms of the concentration reductions,**
- 3) **Basing on the numerical calculations, one can say that the radioactive decay is of a small importance in terms of the concentration reductions.**

Thank you for your attention